

Contents lists available at ScienceDirect

## Journal of Hazardous Materials



journal homepage: www.elsevier.com/locate/jhazmat

# Mixture effects during the oxidation of toluene, ethyl acetate and ethanol over a cryptomelane catalyst

### V.P. Santos, M.F.R. Pereira, J.J.M. Órfão, J.L. Figueiredo\*

Laboratório de Catálise e Materiais (LCM), Laboratório Associado LSRE/LCM, Departamento de Engenharia Química, Faculdade de Engenharia, Universidade do Porto, Rua Dr. Roberto Frias, 4200-465 Porto, Portugal

#### ARTICLE INFO

Article history: Received 4 July 2010 Received in revised form 24 September 2010 Accepted 9 October 2010 Available online 15 October 2010

Keywords: Cryptomelane Oxidation Volatile organic compounds Mixtures

#### ABSTRACT

The catalytic oxidation of two-component VOC mixtures (ethanol, ethyl acetate and toluene) was studied over cryptomelane.

Remarkable mixture effects were observed on the activity and the selectivity. Toluene inhibits both ethyl acetate and ethanol oxidation, this effect being more evident in the case of ethyl acetate. For instance, the temperature for 100% conversion is about 210 °C when ethyl acetate is oxidised alone, and 250 °C or higher, when it is oxidised in mixtures with toluene.

On the contrary, toluene oxidation is only slightly inhibited by the presence of ethyl acetate, while the presence of ethanol has a promoting effect.

Concerning the mixtures of ethyl acetate and ethanol, both compounds have a mutual inhibitory effect, which is more evident in the case of ethyl acetate (the temperature for 100% conversion of ethyl acetate is about 45 °C higher when ethyl acetate is oxidised in mixtures with ethanol, while in the case of ethanol the corresponding increase is only 10 °C).

© 2010 Elsevier B.V. All rights reserved.

#### 1. Introduction

Air pollution is both a local and a trans-boundary problem caused by the emission of certain pollutants that, either alone or by chemical reactions, have negative environmental and health impacts [1].

Volatile organic compounds (VOC) are an important class of air pollutants which covers a wide range of compounds that differ in their properties and chemistry, but display similar behaviour in the atmosphere. The release of VOC into the atmosphere has widespread environmental implications and has been linked to stratospheric ozone depletion, formation of ground level ozone (photochemical smog) and enhancement of the global greenhouse effect [1–3]. Moreover, these compounds require special attention due to their toxicity (human health effects), high stability and persistence in the environment.

The environmental and human health issues have led to a variety of standards and legislation [4]. One of the most important for the European Union is the directive 2001/81/EC (NECD), which establishes ceilings for the emission of certain atmospheric pollutants (SO<sub>2</sub>, NO<sub>x</sub>, VOC and NH<sub>3</sub>) for the different countries, which should be reached by 2010 [4,5]. The aim is to minimize the adverse

effects from acidification, soil eutrophication and ground level ozone.

Catalytic oxidation is a promising technology to control the emissions of volatile organic compounds (VOC) [6]. The key parameter of this process is the type of catalyst used, which is always a function of the VOC and its concentration, the presence of poisons or/and inhibitors, and any inlet temperature constraints.

Industrial emissions usually contain a mixture of VOC with variable composition. The "mixture effect" is very difficult to predict *a priori* [7], as either an inhibition effect [8–10] or (more rarely) a promoting effect [11] can be observed when the components of the mixture are oxidised. In addition, changes in selectivity to by-products have also been observed [8,12–14].

Some authors have pointed out that the inhibition effect can be due to competition between the compounds for adsorption onto the active sites [10,13,15–17]. For example, Tsou et al. [10] observed that the oxidation of methyl-isobutyl-ketone (MIBK) on zeolite supported platinum catalysts was strongly inhibited by the presence of o-xylene, which adsorbs strongly onto the active sites. Moreover, the oxidation of 2-propanol over platinum supported on a monolith was negatively affected by the presence of toluene and methyl-ethyl-ketone (MEK) [8]. This inhibition effect was found to be related to the competition for the oxygen atoms chemisorbed on Pt, and not due to competition for the adsorption sites on the support.

On the other hand, the oxidation of certain compounds can also be independent of the presence of other VOC. For example, the

<sup>\*</sup> Corresponding author. Tel.: +351 22 508 1663; fax: +351 22 508 1449. *E-mail addresses:* santos.vera@fe.up.pt (V.P. Santos), fpereira@fe.up.pt

<sup>(</sup>M.F.R. Pereira), jjmo@fe.up.pt (J.J.M. Órfão), jlfig@fe.up.pt (J.L. Figueiredo).

<sup>0304-3894/\$ -</sup> see front matter © 2010 Elsevier B.V. All rights reserved. doi:10.1016/j.jhazmat.2010.10.036

#### Table 1

Properties of the catalyst: structure (obtained by XRD), surface area (obtained by nitrogen adsorption), average oxidation state (AOS) and relative amount of Mn(IV) surface species (obtained by XPS).

Phase	$S_{\text{BET}}(m^2/g)$	AOS	% Mn(IV)
KMn <sub>8</sub> O <sub>16</sub>	71	3.89	83

presence of n-hexane does not affect the oxidation of benzene and toluene over a Pt/Al<sub>2</sub>O<sub>3</sub> catalyst [18]. It was concluded that the addition of a compound that is more weakly adsorbed on the catalyst than the original one does not affect the reaction rate significantly.

A promoting effect has also been observed in the oxidation of mixtures [11,19,20]. Generally, this effect is a consequence of the higher exothermicity of the process [20]. However, in some systems this effect cannot be explained by heat generation during the reaction. For example, the oxidation of chlorobenzene over a  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalyst [19] is enhanced by the addition of aliphatic hydrocarbons, such as pentane, heptane or decane. Alkanes have the ability to remove Cl from the Pt surface (at the same time reducing the metal), which otherwise would only be removed at higher temperatures, explaining the promoting effect.

The aim of the present work is to study the performance of cryptomelane ( $KMn_8O_{16}$ ) in the oxidation of VOC binary mixtures. Three binary mixtures are studied: ethyl acetate/toluene, ethyl acetate/ethanol and ethanol/toluene.

#### 2. Experimental

#### 2.1. Catalyst synthesis and characterization

Cryptomelane was prepared by the reflux method according to [21]. Briefly, a solution of KMnO<sub>4</sub> (Vaz Pereira, 99% purity) was added to Mn(CH<sub>3</sub>COO)<sub>2</sub> (Fluka, 99% purity) in acidic medium. The initial pH was adjusted to 3.5, using HNO<sub>3</sub> (Panreac, 65% purity). Further details can be found elsewhere [22]. The structure, morphology, composition, manganese average oxidation state (AOS), BET surface area and stability of the prepared samples were fully characterized by X-ray diffraction (XRD), scanning electron microscopy/energy dispersive X-ray spectroscopy (SEM/EDS), Xray photoelectron spectroscopy (XPS), N<sub>2</sub> adsorption at -196 °C, thermogravimetric analysis (TGA) and temperature programmed desorption (TPD) [22,23]. A summary of the main catalyst properties is presented in Table 1.

#### 2.2. Catalytic activity measurements

Ethyl acetate, ethanol and toluene were the VOC chosen for this study. The catalytic oxidation of VOC was performed under atmospheric pressure in a fixed-bed reactor from Autoclave Engineers (BTRS Jr), which consists of a stainless steel tube of 6 mm internal diameter, placed inside a temperature-controlled electric furnace. A feed gas with selected VOC inlet concentrations and a space velocity of  $16,000 h^{-1}$  was used. The catalyst sample (50 mg) was diluted with glass spheres of the same size as the catalyst particles (0.2–0.5 mm), in order to minimize temperature gradients.

Conversions were measured over the range 100-350 °C by incremental steps (10-20 °C), the temperature being measured by a thermocouple placed in the middle of the catalyst bed. To ensure that steady state data were measured, the reactor was maintained at each temperature for 30 min. The conversion of VOC (*X*) was calculated as

$$X = 1 - \frac{F_{\rm VOC}}{F_{\rm VOC,in}}$$



Fig. 1. Conversion of ethyl acetate alone (1600 ppmv), and in binary mixtures with toluene.

where  $F_{VOC}$  is the outlet molar flow rate of VOC at steady state and  $F_{VOC,in}$  is the inlet molar flow rate of VOC. Further details can be found elsewhere [22].

#### 3. Results and discussion

The catalytic performance of cryptomelane in the single oxidation of ethanol, ethyl acetate and toluene was previously studied [22–25]. Cryptomelane was found to be very active, promoting the oxidation of these VOC at relatively low temperatures. The conversion level was influenced by the type of VOC, the reactivity into  $CO_2$ increasing in the following order: toluene < ethanol < ethyl acetate.

The oxidation process of the oxy-derivative compounds was found to be more complex than that of toluene, yielding not only  $CO_2$  and  $H_2O$ , but also partially oxidised intermediates (namely acetaldehyde). On the other hand, it was established that lattice oxygen is involved in the oxidation process of all VOC studied, suggesting a Mars and van Krevelen mechanism [23]. In this context, the type of VOC is particularly important, as it dictates the reduction of the catalyst and, consequently, the rate of oxygen incorporation in the lattice, which explains the lower reactivity observed with toluene.

In the present work, the performance of cryptomelane in the oxidation of three binary mixtures was evaluated.

#### 3.1. Ethyl acetate/toluene mixtures

The activity of cryptomelane in the oxidation of ethyl acetate/toluene mixtures was evaluated by performing two sets of experiments. In the first one, the concentration of one of the components was kept constant, while the concentration of the other component was changed within a pre-established range (see Figs. 1 and 2). The second type of experiment was carried out by changing the relative proportions of toluene and ethyl acetate in the mixture, while keeping the concentration of carbon in the feed constant (see Fig. 3).

Fig. 1 shows the effect of toluene on ethyl acetate oxidation. It can be observed that the presence of toluene strongly inhibits the oxidation of ethyl acetate, and this effect increases with the toluene concentration, being particularly important for 1600 ppmv. For instance, the temperature for 100% conversion is about 210 °C when ethyl acetate is oxidised alone, and 250 °C or higher, when it is oxidised in mixtures with toluene. On the other hand, it can be observed (see Fig. 2) that ethyl acetate does not have a significant effect in the oxidation of toluene. This result was already expected,



Fig. 2. Conversion of toluene alone (1600  $\ensuremath{\mathsf{ppmv}}\xspace$ ), and in binary mixtures with ethyl acetate.

since ethyl acetate is oxidised almost completely before toluene conversion starts (see Fig. 3).

Fig. 3 shows the results obtained in the second set of experiments, as well as the corresponding calculated curves (obtained by averaging the oxidation temperatures of the individual compounds accordingly to the respective proportions in the mixture). As can be seen, the light-off curves of the mixtures have an intermediate behaviour in comparison to the two compounds alone. The experimental curves follow the calculated ones initially, while toluene is not converted. However, significant discrepancies between these curves and the calculated ones occur in the range of temperatures where toluene is converted, showing an inhibition effect. Moreover, it can be observed that the temperature necessary for the total conversion into  $CO_2$  is determined by the corresponding temperature of the less reactive compound.

Similar conclusions have been reported by other authors [8-10,12,13,15-17]. In general, the inhibition effects can be a result of the competition between the compounds for the adsorption sites [10,13,15-17], or/and the competition for oxygen atoms [8,12]. In a previous work [23], it was shown that the interaction of the oxy-derivative compounds with cryptomelane differs greatly from



**Fig. 3.** Conversion into CO<sub>2</sub> ( $X_{CO_2}$ ) of the individual compounds and ethyl acetate/toluene mixtures, defined as:  $X_{CO_2} = F_{CO_2}/F_{carbon,in}$ , where  $F_{CO_2}$  is the outlet molar flow rate of CO<sub>2</sub> at steady state and  $F_{carbon,in}$  is the inlet molar flow rate of carbon. The concentration of carbon in the feed is 4000 ppm. The calculated curves for the mixtures (obtained by averaging the oxidation temperatures of the individual compounds accordingly to the respective proportions in the mixture) are also represented.



**Fig. 4.** (a) Conversion of ethanol alone (3700 ppmv) and in a binary mixture with toluene. (b) Corresponding conversion into acetaldehyde, defined as:  $X_{\text{Acetal}} = F_{\text{Acetal}} / F_{\text{Ethanol,in}}$ , where  $F_{\text{Acetal}}$  is the outlet molar flow rate of acetaldehyde at steady state.

toluene. Toluene has a strong affinity with the catalyst surface, being retained up to high temperatures (temperatures higher than the reaction temperature). The accumulation of these molecules on the catalyst structure was found to be at the origin of an oscillatory behaviour [24]. On the other hand, cryptomelane is not able to retain ethyl acetate at high temperatures. These results suggest that toluene is more strongly adsorbed than ethyl acetate, and the inhibition effect can result from the competition of both compounds for the active sites. It should be noted that the inhibition effect observed for ethyl acetate oxidation (in the first set of experiments) cannot be explained by the presence of higher amounts of H<sub>2</sub>O and CO<sub>2</sub>, since it was previously established that the oxidation of ethyl acetate is not affected by the presence of these compounds [22].

#### 3.2. Ethanol/toluene mixtures

The results concerning ethanol/toluene mixtures are shown in Figs. 4 and 5. It can be observed (see Fig. 4a) that ethanol conversion is also inhibited by the presence of toluene, but to a lesser extent comparatively to ethyl acetate. Concerning acetaldehyde production (see Fig. 4b), it was observed that the presence of toluene slows down the partial oxidation of ethanol to acetaldehyde, shifting the curve to higher temperatures. However, the maximum amount of acetaldehyde produced in the individual oxidation of ethanol is lower than that produced in the oxidation of the mixture. This effect was also observed by other authors [8,12].



Fig. 5. Conversion of toluene alone  $(1600\,\text{ppmv})$  and in binary mixtures with ethanol.

The effect of ethanol on the conversion of toluene is shown in Fig. 5. A slight promoting effect seems to occur, since the corresponding light-off curves are shifted to lower temperatures at high conversions. This effect increases with the concentration of ethanol. For instance, the temperature for 100% conversion is about 300 °C when toluene is oxidised alone, and lower than 285 °C when it is oxidised in the mixtures with ethanol tested. This effect is most probably a consequence of the higher exothermicity of the process when the mixtures are considered.

It should be remarked that, when toluene starts to oxidise, ethanol has already been transformed into acetaldehyde and CO<sub>2</sub> (minor amounts); so significant amounts of this intermediate compound are present. For this reason, the behaviour of this mixture should be similar to the acetaldehyde/toluene mixture.

#### 3.3. Ethanol/ethyl acetate mixtures

The mutual influence of the components of a binary mixture may be more interesting when the oxidation reactions of both compounds alone take place in the same temperature range, as in the case of ethyl acetate/ethanol mixtures (Figs. 6 and 7).

Regarding the effect of ethanol concentration on ethyl acetate oxidation (see Fig. 6), it can be seen that the presence of ethanol clearly inhibits the oxidation of ethyl acetate, shifting the light-off



Fig. 6. Conversion of ethyl acetate alone (1600 ppmv) and in a binary mixture with ethanol.



**Fig. 7.** (a) Conversion of ethanol alone (1600 ppmv) and in a binary mixture with ethyl acetate. (b) Corresponding conversions into acetaldehyde.

curve to higher temperatures. The temperature for 100% conversion is about 45 °C higher.

Fig. 7 shows the effect of the presence of ethyl acetate on ethanol oxidation. It can be observed that ethyl acetate also inhibits the partial oxidation of ethanol, decreasing the conversion into acetaldehyde. However, this effect is not as evident as with the addition of ethanol to ethyl acetate.

In summary, there is a mutual inhibition effect between ethanol and ethyl acetate, although this effect is much more evident in ethyl acetate combustion. These results can be explained by the competition for the adsorption sites, because both compounds are polar, which results in a similar interaction with the catalyst surface. Moreover, a similar mechanism can take place in the oxidation of both compounds. Acetaldehyde can also play a key role on the inhibition effects observed, as it is the major intermediate in ethanol oxidation.

#### 4. Conclusions

The following conclusions can be drawn from this study:

- Cryptomelane was found to be very active in the oxidation of VOC and its mixtures.
- Toluene affects both ethyl acetate and ethanol oxidation. This effect is much more evident in the case of ethyl acetate (the temperature shift for 100% conversion is higher than 40  $^\circ$ C when

ethyl acetate is oxidised in mixtures). The inhibition effect can be explained by the competition between the compounds for the adsorption sites.

- Toluene oxidation is not significantly affected by the presence of ethyl acetate, while the presence of ethanol has a slight promoting effect (mainly due to the oxidation of acetaldehyde), which was attributed to a local heating effect.
- Concerning ethyl acetate and ethanol mixtures, it was observed that these compounds have a mutual inhibitory effect, which is much more evident in the case of ethyl acetate oxidation (the temperature for 100% conversion of ethyl acetate is about 45 °C higher when ethyl acetate is oxidised in mixtures with ethanol, while in the case of ethanol the corresponding increase is only 10 °C).

#### Acknowledgements

This work was supported by Fundação para a Ciência e a Tecnologia (FCT) and FEDER under Programme COMPETE (project PTDC/AMB/69065/2006). V.P.S. acknowledges the grant received from FCT (SFRH/BD/23731/2005).

#### References

- R.J. Heinsohn, R.L. Kabel, Sources and Control of Air Pollution, Prentice Hall, Upper Saddle River, NJ, 1999.
- [2] T.F. Garetto, I. Legorburu, M. Montes, Eliminación de emisiones atmosféricas de COVs por catálisis y adsorción, CYTED, 2008.
- [3] R.E. Hester, R.M. Harrison, Volatile Organic Compounds in the Atmosphere, Royal Society of Chemistry, 1995.
- [4] M. Amann, M. Lutz, The revision of the air quality legislation in the European Union related to ground-level ozone, J. Hazard. Mater. 78 (2000) 41–62.
- [5] EU Council Directive 2001/81/EC of 23 October 2001.
- [6] E.C. Moretti, N. Mukhopadhyay, VOC control-current practices and future trends, Chem. Eng. Prog. 89 (1993) 20–26.
- [7] J.J. Spivey, Complete catalytic oxidation of volatile organics, Ind. Eng. Chem. Res. 26 (1987) 2165–2180.
- [8] N. Burgos, M. Paulis, M.M. Antxustegi, M. Montes, Deep oxidation of VOC mixtures with platinum supported on Al<sub>2</sub>O<sub>3</sub>/Al monoliths, Appl. Catal. B-Environ. 38 (2002) 251–258.

- [9] A. Musialik-Piotrowska, K. Syczewska, Catalytic oxidation of trichloroethylene in two-component mixtures with selected volatile organic compounds, Catal. Today 73 (2002) 333–342.
- [10] J. Tsou, P. Magnoux, M. Guisnet, J.J.M. Órfão, J.L. Figueiredo, Catalytic oxidation of volatile organic compounds—oxidation of methyl-isobutyl-ketone over Pt/zeolite catalysts, Appl. Catal. B-Environ. 57 (2005) 117–123.
- [11] S. Irusta, M.P. Pina, M. Menéndez, J. Santamaría, Catalytic combustion of volatile organic compounds over La-based perovskites, J. Catal. 179 (1998) 400–412.
- [12] F.N. Aguero, B.P. Barbero, L. Gambaro, L.E. Cadus, Catalytic combustion of volatile organic compounds in binary mixtures over MnO<sub>x</sub>/Al<sub>2</sub>O<sub>3</sub> catalyst, Appl. Catal. B-Environ. 91 (2009) 108–112.
- [13] A. Musialik-Piotrowska, K. Syczewska, Combustion of volatile organic compounds in two-component mixtures over monolithic perovskite catalysts, Catal. Today 59 (2000) 269–278.
- [14] L. Wang, M. Sakurai, H. Kameyama, Catalytic oxidation of dichloromethane and toluene over platinum alumite catalyst, J. Hazard. Mater. 154 (2008) 390–395.
- [15] V. Blasin-Aubé, J. Belkouch, L. Monceaux, General study of catalytic oxidation of various VOCs over La<sub>0.8</sub>Sr<sub>0.2</sub>MnO<sub>3+x</sub> perovskite catalyst-influence of mixture, Appl. Catal. B-Environ. 43 (2003) 175–186.
- [16] I. Mazzarino, A.A. Barresi, Catalytic combustion of VOC mixtures in a monolithic reactor, Catal. Today 17 (1993) 335–347.
- [17] P. Papaefthimiou, T. Ioannides, X.E. Verykios, Performance of doped Pt/TiO<sub>2</sub> (W<sup>6+</sup>) catalysts for combustion of volatile organic compounds (VOCs), Appl. Catal. B-Environ. 15 (1998) 75–92.
- [18] S. Ordóñez, L. Bello, H. Sastre, R. Rosal, F.V. Díez, Kinetics of the deep oxidation of benzene, toluene, n-hexane and their binary mixtures over a platinum on γ-alumina catalyst, Appl. Catal. B-Environ. 38 (2002) 139–149.
- [19] R.W. van den Brink, P. Mulder, R. Louw, Catalytic combustion of chlorobenzene on Pt/γ-Al<sub>2</sub>O<sub>3</sub> in the presence of aliphatic hydrocarbons, Catal. Today 54 (1999) 101–106.
- [20] A.A. Barresi, G. Baldi, Deep catalytic oxidation of aromatic hydrocarbon mixtures: reciprocal inhibition effects and kinetics, Ind. Eng. Chem. Res. 33 (1994) 2964–2974.
- [21] J. Luo, Q. Zhang, A. Huang, S.L. Suib, Total oxidation of volatile organic compounds with hydrophobic cryptomelane-type octahedral molecular sieves, Micropor. Mesopor. Mater. 35–36 (2000) 209–217.
- [22] V.P. Santos, M.F.R. Pereira, J.J.M. Órfão, J.L. Figueiredo, Synthesis and characterization of manganese oxide catalysts for the total oxidation of ethyl acetate, Top. Catal. 52 (2009) 470–481.
- [23] V.P. Santos, M.F.R. Pereira, J.J.M. Órfão, J.L. Figueiredo, The role of lattice oxygen on the activity of manganese oxides towards the oxidation of VOC, Appl. Catal. B-Environ. 99 (2010) 353–363.
- [24] V.P. Santos, S.S.T. Bastos, M.F.R. Pereira, J.J.M. Órfão, J.L. Figueiredo, Stability of a cryptomelane catalyst in the oxidation of toluene, Catal. Today 154 (2010) 308–311.
- [25] V.P. Santos, M.F.R. Pereira, J.J.M. Órfão, J.L. Figueiredo, Catalytic oxidation of ethyl acetate over a cesium modified cryptomelane catalyst, Appl. Catal. B-Environ. 88 (2009) 550–556.